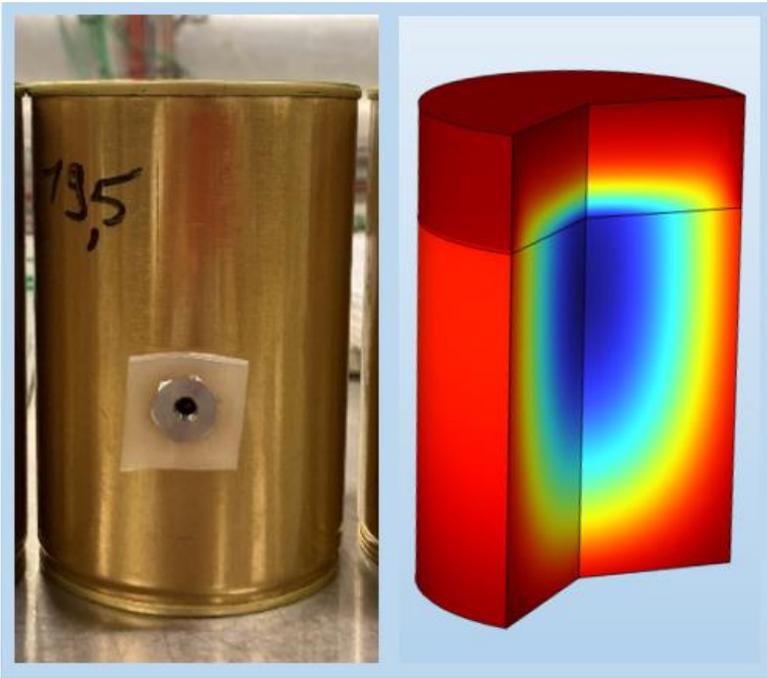


CFD-based Approach For Prediction Of Headspace Pressure In Can During Thermal Sterilization Of Foods



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Context

What is Thermal Sterilization?



Raw Food



Thermal sterilization using Retort

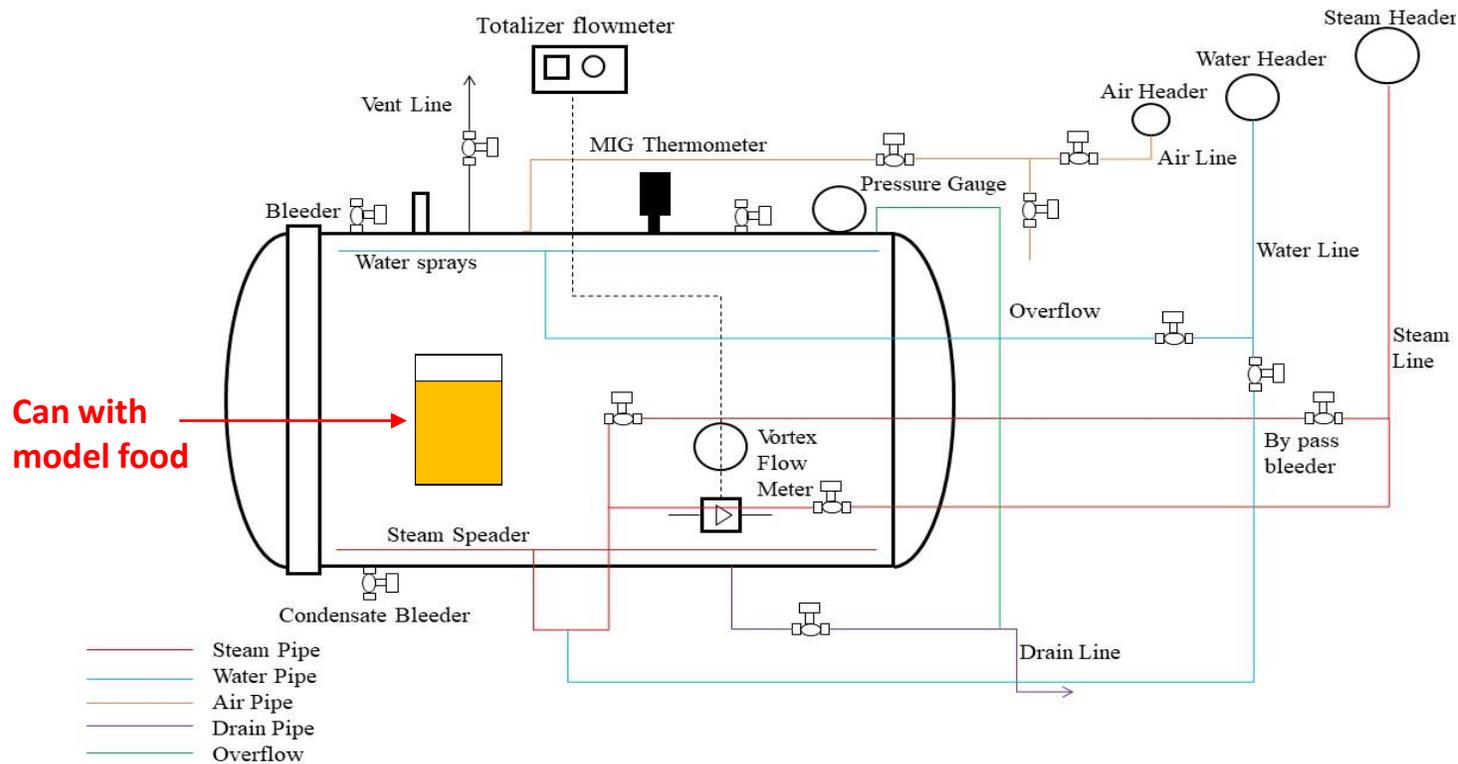
- Heat treatment above 100°C
- Destroys heat-resistant spores



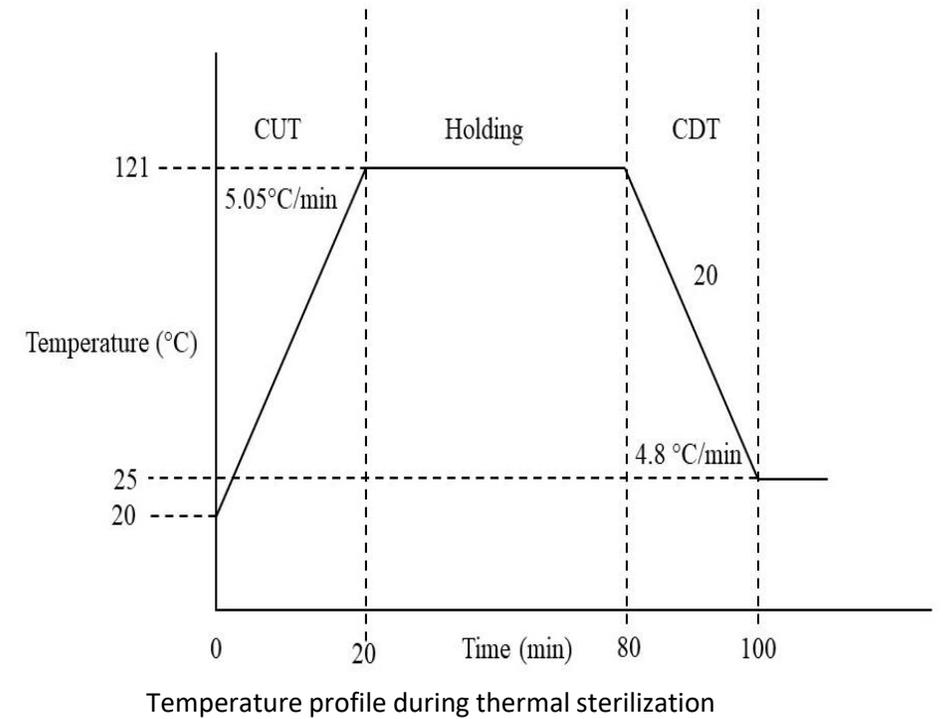
Canned Foods with longer shelf life (eg. ≥ 2 years)



Retort Overview

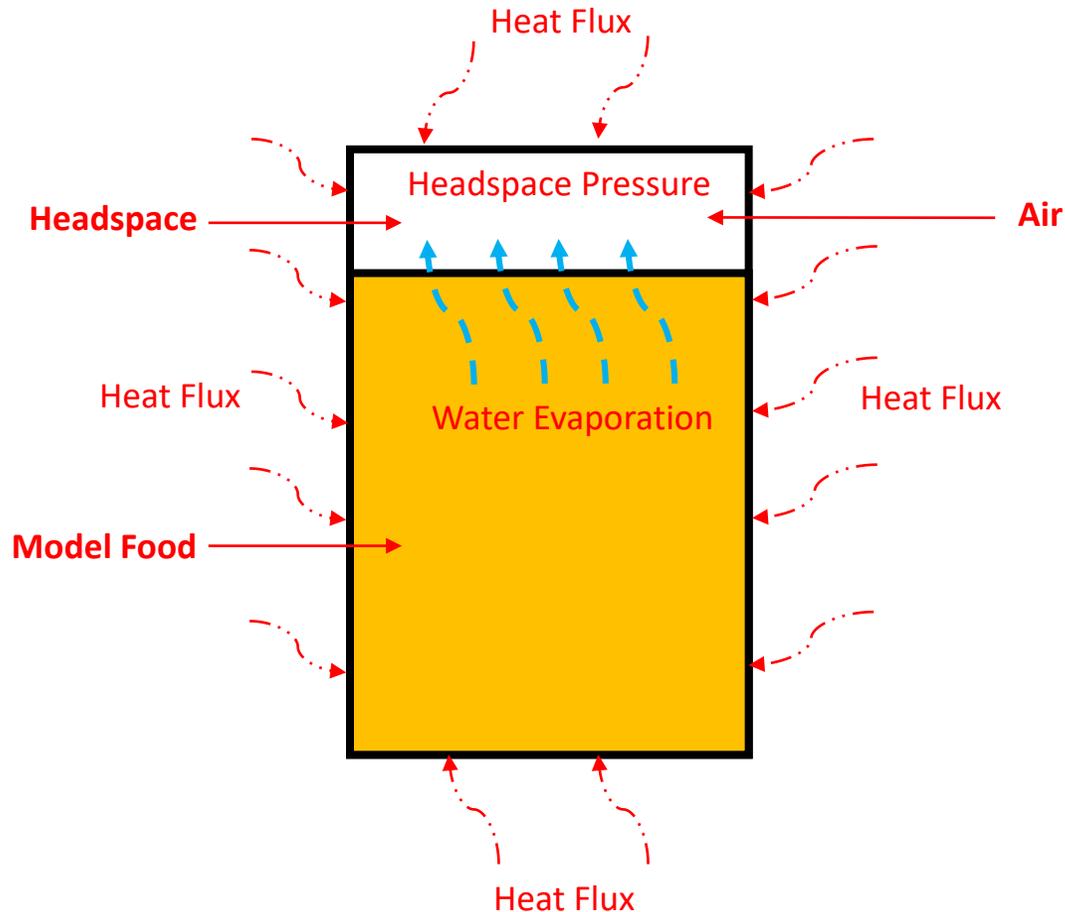


Schematic of a conventional retort for thermal sterilization



Challenge and Goal

Headspace Pressure



Challenge

- **Measuring headspace pressure due to water vapour in the food industry is a big challenge.**
- External counter-pressure is required to tackle **inner pressure** generated in canned foods which is related to headspace pressure.

Goal

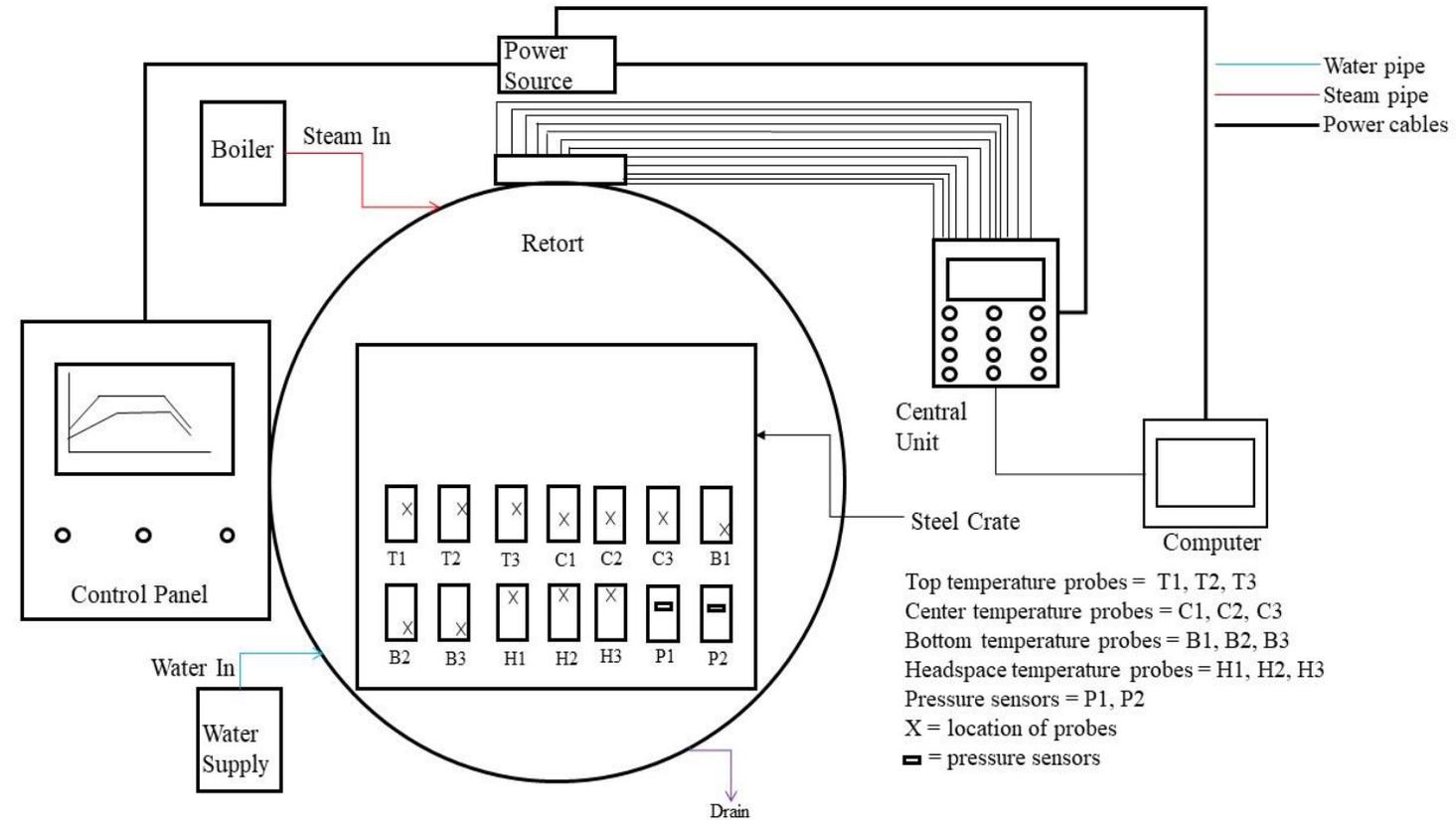
- To predict **local temperatures** and **internal headspace pressure** in cans during thermal sterilization process, which accounts for **water vapor generation and dry air pressure in the headspace.**

Materials and Methods

Experimental Setup



STERITECH Retort in Oniris, Nantes, France



Schematic of experimental setting



Materials and Methods

Experimental Setup



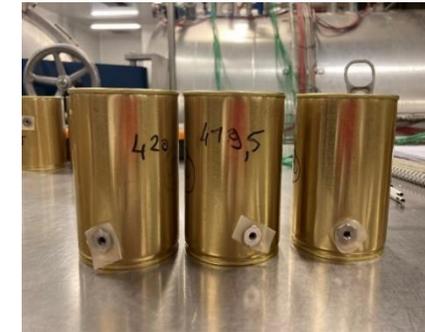
3 cans for top temperature



3 cans for center temperature



3 cans for headspace temperature



3 cans for bottom temperature

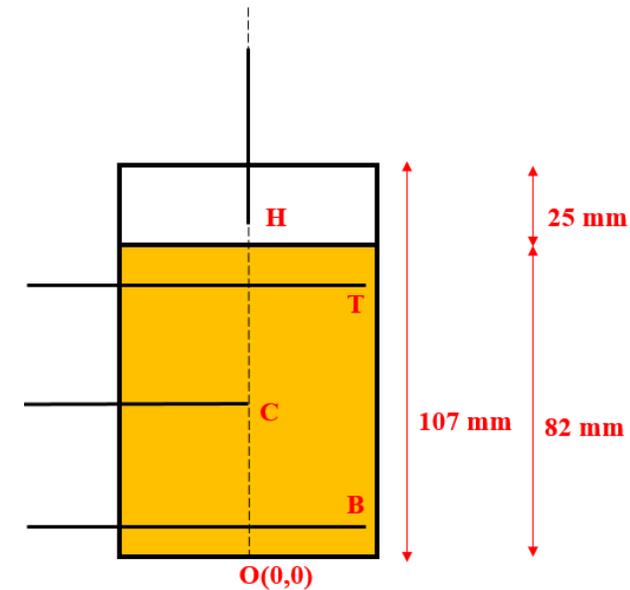
Mass of mashed potato
= 279.96 ± 0.42 g



Temperature probes



Pressure sensor inside cans



Location of temperature probes in the cans



Numerical Modelling: Governing Equations

Heat Transfer in Solids (mashed potato)

$$\rho C_p \frac{\partial T}{\partial t} - \nabla \cdot (-k \nabla T) = 0 \quad (1)$$

+Initial Conditions +Boundary Conditions

$$T_{initial} = 20^\circ C$$

$$-n \cdot q = q_0 \quad (2)$$

$$q_0 = h_{global}(T_{retort} - T) \quad (3)$$

Heat Transfer in Fluids (air at the headspace)

$$\rho C_p \frac{\partial T}{\partial t} + \rho C_p \mathbf{u} \cdot \nabla T - \nabla \cdot (k \nabla T) = 0 \quad (4)$$

+Initial Conditions + Boundary Conditions

Fluid Mechanics : Navier-Stokes equations with the Boussinesq approximation (air at the headspace)

$$\rho \frac{\partial \mathbf{u}}{\partial t} = -\nabla p + \mu \nabla^2 \mathbf{u} + F \quad (5)$$

$$F = \rho g \quad (6)$$

+Initial Conditions +Boundary Conditions

$$p = 1 \text{ [atm]}$$

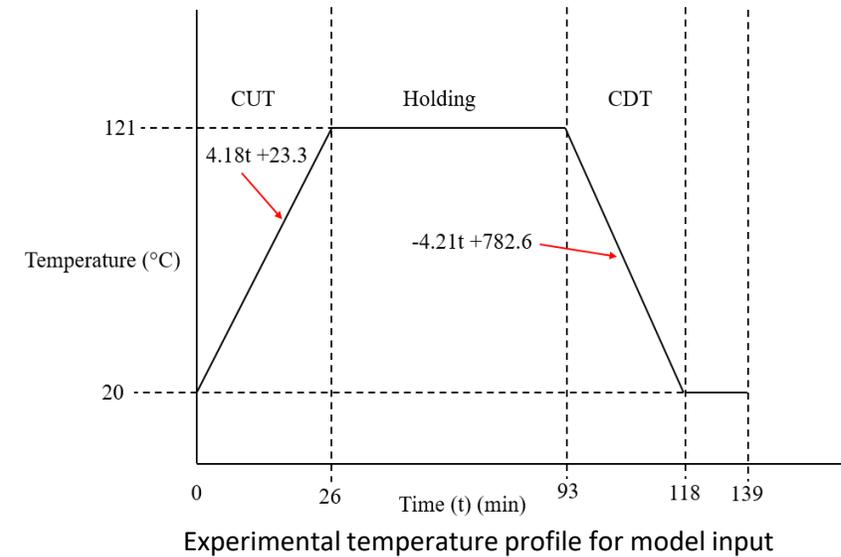
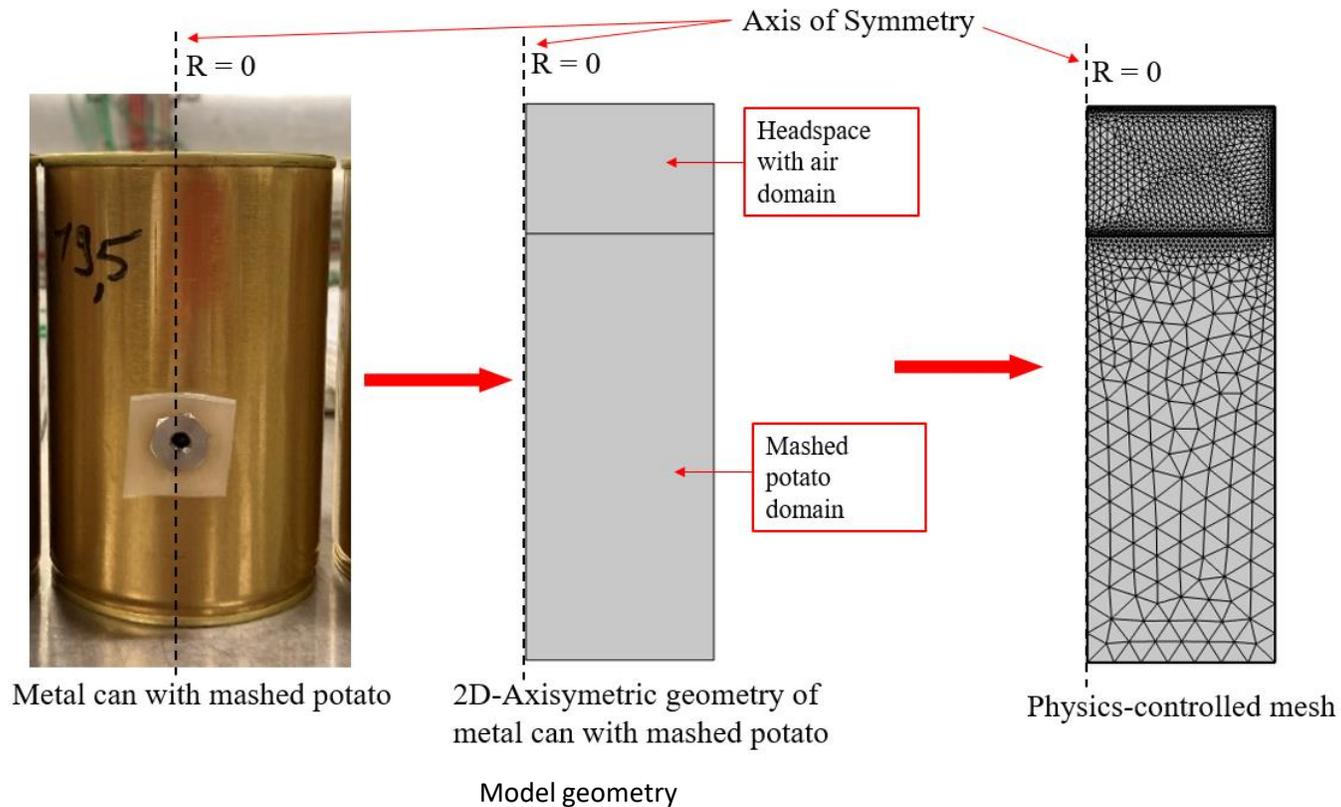
$$\mathbf{u}_{initial} = \mathbf{0} \quad (7)$$

Ideal gas law for dry air at the headspace

$$PV = nRT \quad (8)$$



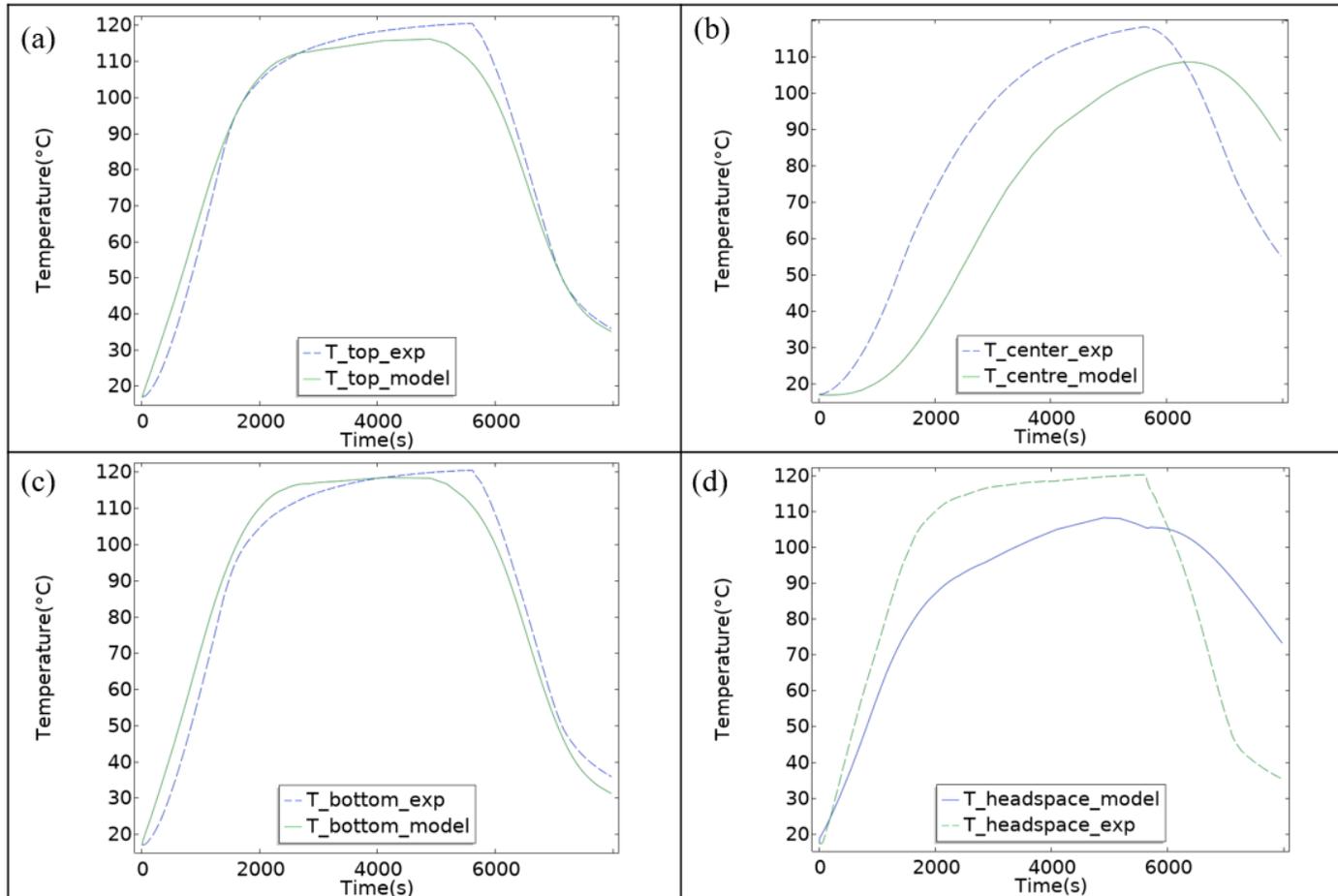
COMSOL Modelling: Implementation



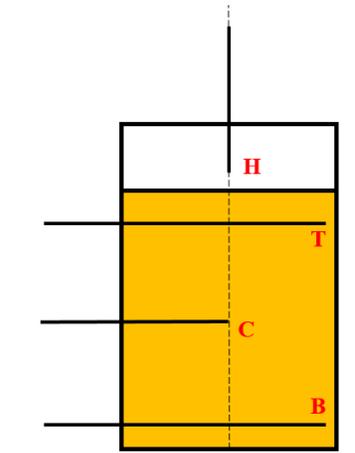
Parameters		Values
Density of model food (mashed potato)	ρ_{mp}	1052.96 kg/m ³
Thermal conductivity of model food (mashed potato)	k_{mp}	0.55 W/m/K
Specific heat capacity model food (mashed potato)	Cp_{mp}	0.0576 T ² - 33.551 T + 8445.2 J/kg/K
Density of metal can	ρ_{can}	7900 kg/m ³
Thermal conductivity of metal can	k_{can}	45 W/m/K
Specific heat capacity of metal can	Cp_{can}	213 J/kg/K



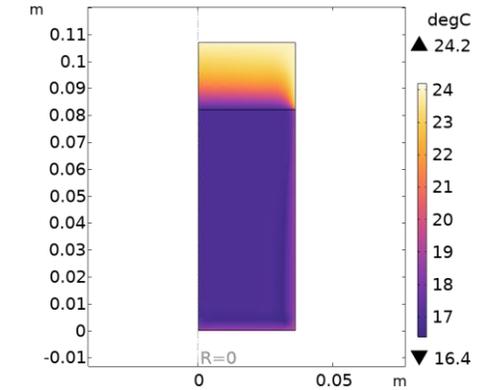
Temperature evolution



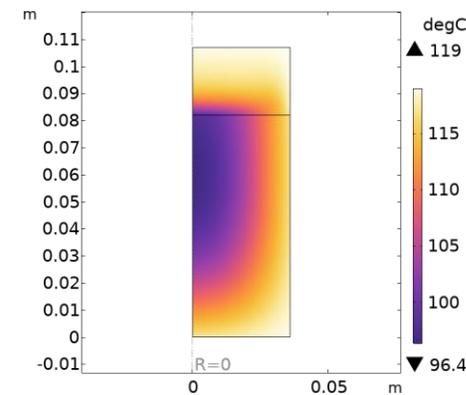
Experimental and simulated temperature profile at (a) Top location (b) Center location (c) Bottom location (d) Headspace location.



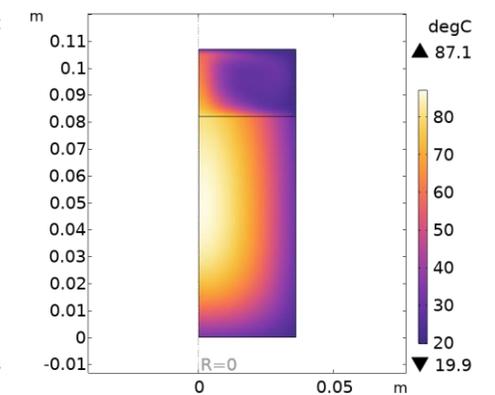
Location of temperature measurement



Temperature distribution at 10 s



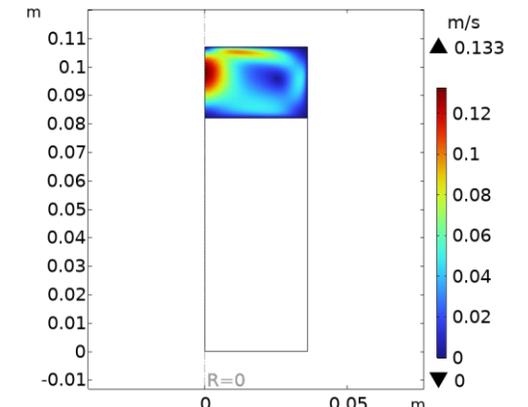
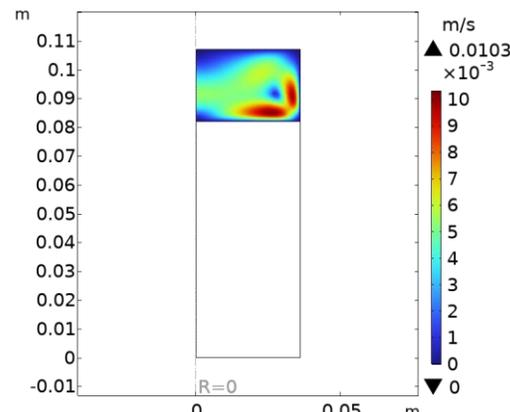
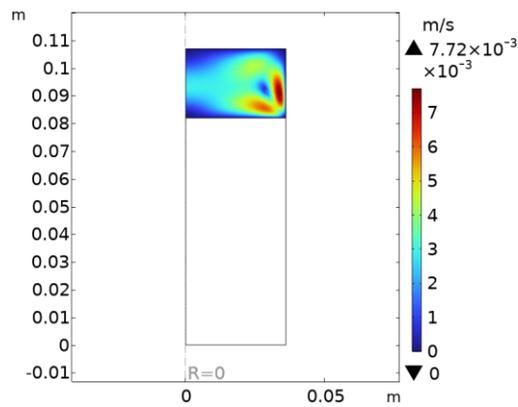
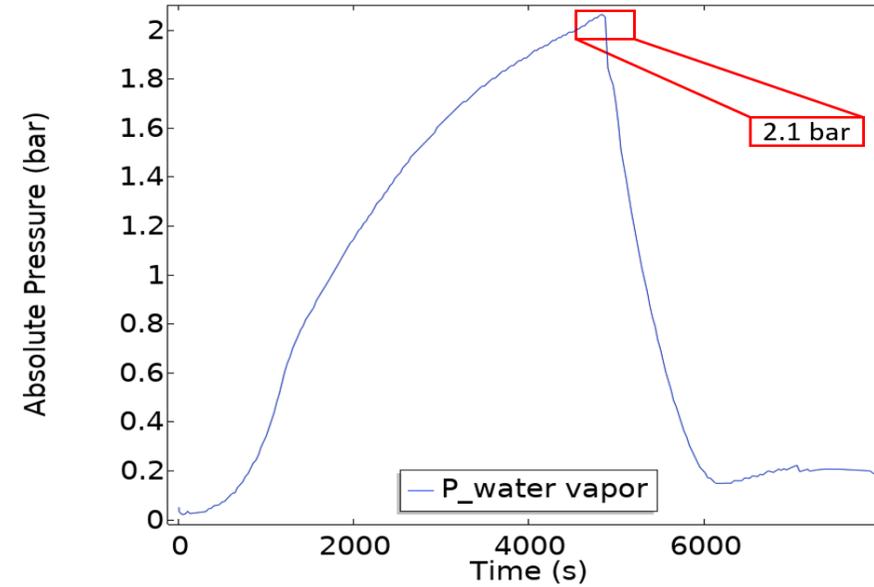
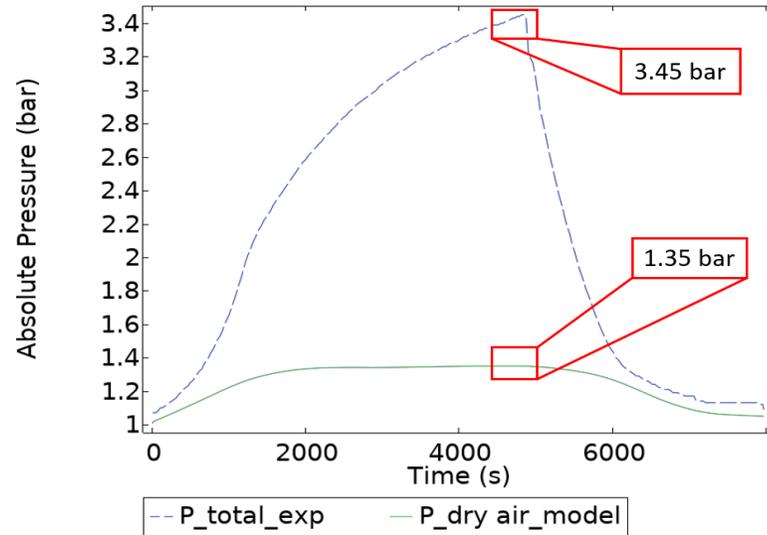
Temperature distribution at 4821 s



Temperature distribution at 7968 s

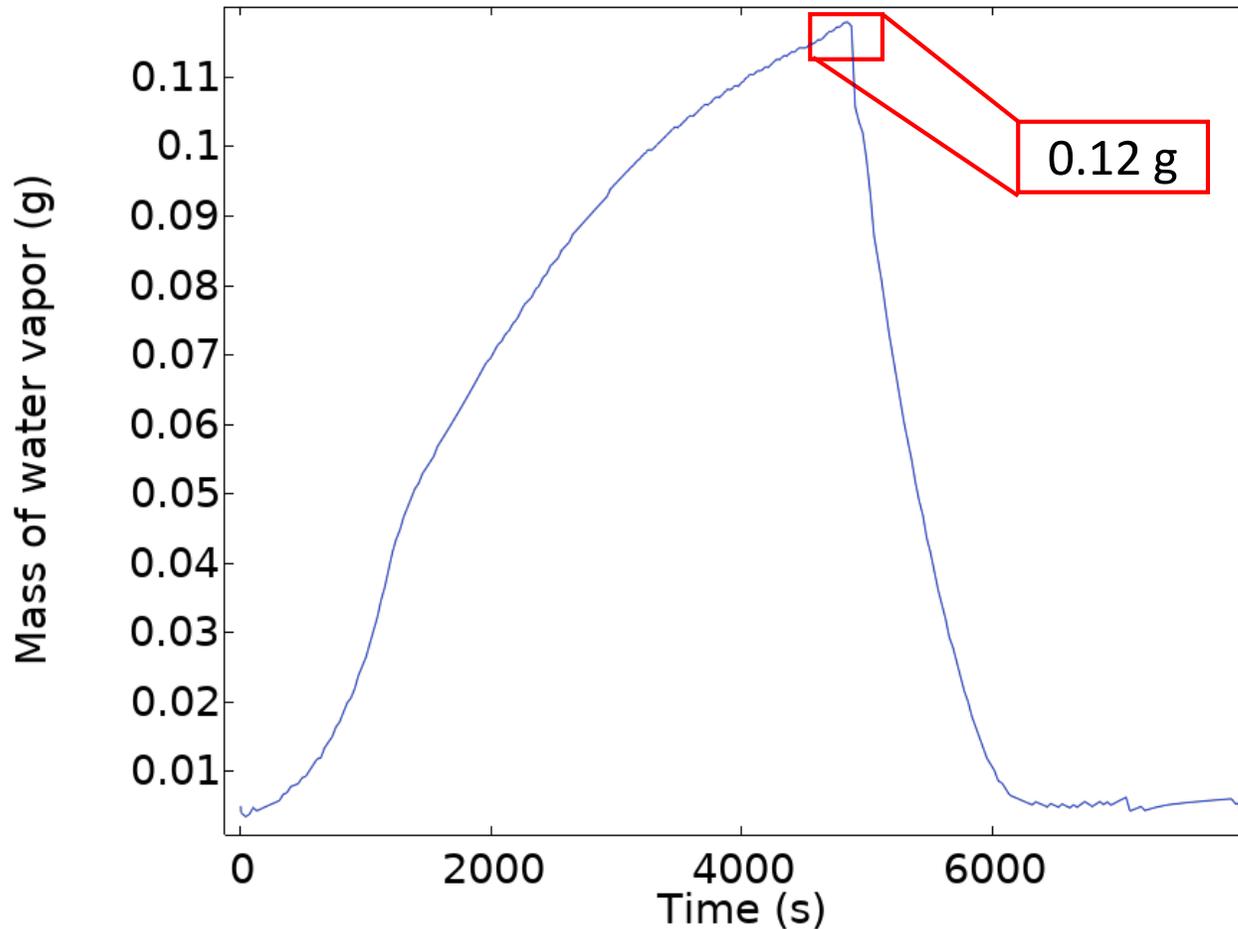


Pressure and Velocity





Water Vapour Generation



$$P_{air}V_{headspace} = n_{air}RT$$

$$P_{vapour}V_{headspace} = n_{vapour}RT$$

$$P_{total} = P_{air} + P_{vapour}$$

Experimental measurement for water vapour generation was of the same order of magnitude: **less than 0.5 g**

Conclusions and Perspectives

The numerical model coupled to the experimental investigation enables to:

- Predict **local temperature profiles at different locations** in canned foods.
- Predict **dry air pressure in the headspace**.
- Estimate the **water vapour pressure** contributing towards headspace pressure
- Evaluate the **mass of water vapour generated** during the thermal sterilization process.

Perspectives

- Improvement of the numerical model by integrating water vapour evaporation flux in the CFD model.



Thank You Very Much For Your Attention

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