

# **Simulating the Coupled Mass and Heat Transport in Package Material during Induction Sealing**

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- − Tetra Pak, Tetra Pak® Package Material, Induction Sealing
- ► Package material model: heat and mass transport
- ► Induction heating device model
- ▶ Results & discussion



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## **Tetra Pak A world leading food processing and packaging company**

### **Packaging technology: design and engineering of Filling Machines**

- Automated machines; from package material reels to liquid food containers in the order of *thousands-per-hour*
- Stored food must stay *fresh and safe for consumption for 1 year* without the need for preservatives or refrigeration







# **Filling machines, package material, induction sealing**

Sterilization, Forming, Filling, Sealing, Cutting | Rackage Material: multi-layered | Paperboard: Porous, Hygroscopic







**Induction sealing is deeply impacted by paperboard physics**

- Heating  $\rightarrow$  Drying  $\rightarrow$  Energy
- Heating  $\rightarrow$  Vapour  $\rightarrow$  Pressure

#### **Induction sealing process**

Exploit high electrical conductivity of Al-foil (eddy current) to heat-up the polyethylene for polymer welding. **Typically: up to 150** ℃ **in < 1 s.**



#### **Next**

Recrystallization

• How is induction heating of package material affected by board properties?



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# **Package material model: heat and mass transport**





[2] H. Askfelt and M. Ristinmaa, "Experimental and numerical analysis of adhesion failure in moist packaging material during excessive heating," International Journal of Heat and Mass Transfer, vol. 108, pp. 2566 - 2580, 2



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# **Induction heating device model (2-D)**





# **Induction heating device model (2-D)**



Contour lines: Az  $[Wb \cdot m^{-2}]$ 





Normalized electromagnetic surface loss. density vs. coordinate

**Excitation: load power (~650 W) ; 600 ms of on-time (Frequency –Transient)**

• Next: sensitivity analysis vs. board initial moisture ratio and density



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Inside

Time-evolution at the board/laminate interface, above the coil active area

 $-1$ 

 $-1.5$ 

 $-2$ 

 $-2.5$ 

 $-3$ 





22.7

20.9

17.4

13.8

10.2

6.61

 $0.1$ 

90  $\frac{1}{300}$  Time (ms)<sup>2</sup> 100 200 400 500  $\omega^0$ =0.04,  $\rho^c$ =500 -  $\omega^0$ =0.04,  $\rho^c$ =700 -  $\omega^0$ =0.04,  $\rho^c$ =900  $\omega^0$  = 0.07,  $\rho^c$  = 500 .......  $\omega^0$  = 0.07,  $\rho^c$  = 700 .......  $\omega^0$  = 0.07,  $\rho^c$  = 900  $\omega^0 = 0.1$ ,  $\rho^c = 500$  -  $-\omega^0 = 0.1$ ,  $\rho^c = 700$  -  $-\omega^0 = 0.1$ ,  $\rho^c = 900$ 

Maximum t

100

Evolution of the maximum temperature of the package material inside top surface



# **Discussion**

### **- Model vs. experimental data carried out on a given board grade**



Max. temperature on inside top surface vs. time





#### *FLIR cooled camera*

- Matching between model and data [1] currently is **not** satisfactory
- Prediction improved with temperature-dependent heat transport parameters of PE
- The model can be used in its present state for **relative comparisons** and to study **interplay of physical parameters**
- COMSOL Multiphysics® as **enabling technology** to allow the collaboration of modeling engineers having different expertise (e.g., paperboard physics / electromagnetic modeling)



### Key takeaways

With COMSOL we are able to simulate the package material response during induction heating.

The model is able to capture complex multiphysical couplings such as gauge pressure build up and drying

> The model may be used to understand how different attributes of the board will affect the package material behavior

Next step

Improve polymer model

- Heat transport & phase transformation





# **Backup Slides**





## **Model Results - Sensitivity analysis**



#### Parametric sweep **Parameter Value list Unit**  $\omega^0$  $0.04, 0.07, 0.1$  $\rho^c$ 500, 700, 900 kg · m<sup>-3</sup>

initial density initial moisture ratio



Max. temperature on inside top surface vs. time

- Lower PE temperature for higher density board
	- higher specific heat
	- higher thermal conductivity
- Lower PE temperature the higher the moisture content
	- higher specific heat
	- higher thermal conductivity
	- more energy required to dry



## **Model Results - Sensitivity analysis**



#### Parametric sweep **Parameter** | **Value list** | **Unit**  $\omega^0$  $0.04, 0.07, 0.1$  $\rho^c$ 500, 700, 900 | kg · m<sup>-3</sup>

#### initial density initial moisture ratio

Max drying over paperboard domain (end of heating phase)

- located on top left corner of board below Al-foil nearby active area
- higher for higher initial moisture ratio  $\rightarrow$  more desorption
	- increased driving force for drying
- higher for decreased density  $\rightarrow$  increased gas volume
	- gas accumulates more water
	- ease for vapor to flow within the board

Max internal pressure build-up over paperboard domain (end of heating phase)

- higher initial moisture  $\rightarrow$  more desorption
- increased density  $\rightarrow$  less desorption
	- increase resistance for gas to flow  $\rightarrow$  higher pressure  $\rightarrow$  higher desorption BUT
	- increased density  $\rightarrow$  lower temperature  $\rightarrow$  lower pressure  $\rightarrow$  lower desorption
- $\triangleright$  decreased temperature dominates over higher mass flux resistivity



 $\mathbf{0}$ 

 $-1$ 

 $-2$ 

 $-3$ 



#### initial density initial moisture ratio





#### **Boundary conditions**

The mass fluxes,  $J_{g_i}^n$ , of the gas constituents, through the free edges of the board (vertical edges in Figure 3), are approximated by stagnant-film models with the incorporation of Stefan correction factors, as described in [7]. No heat flux is assumed on the contact between the biadhesive tape and the aluminum coil. All boundaries between polymers and ambient air assume a Newton cooling format with the heat convection coefficient,  $h_{\alpha}$ , retrieved from classic boundary layer theory. The heat flux,  $q_\theta^n$ , through the free edges of the board, incorporates the mass flux and is given by

$$
q_\theta^n = h_\alpha(\theta - \theta^*) + J_{g_\nu}^n \cdot h_{g_\nu} + J_{g_\alpha}^n \cdot h_{g_\alpha}
$$

where  $h_{g_i}$  [J/kg] is the specific enthalpy of  $g_v$ .